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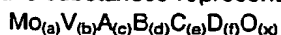
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(54) Catalyst for oxidation of acrolein and process for production thereof.

(57) A catalyst for use in the production of acrylic acid by catalytic gas phase oxidation of acrolein, comprising active substances represented by general formula



wherein Mo represents molybdenum, V represents vanadium, A represents at least one element selected from the group consisting of tungsten and niobium, B represents at least one element selected from the group consisting of iron, copper, bismuth, chromium, antimony and thallium, C represents at least one element selected from the group consisting of alkali metals and alkali earth metals, D represents at least one element selected from the group consisting of silicon, aluminum and titanium, and O represents oxygen; and further, a, b, c, d, e, f and x represent atomic ratios of Mo, V, A, B, C, D, and O respectively, and when a = 12, then b = 2 to 14, c = 0 to 12, d = 0 to 6, e = 0 to 6 and f = 0 to 30 and x is a numerical value determined depending upon the oxidation states of the other elements, and characterized by having a specific surface area of 0.50 to 15.0 m²/g, a pore volume of 0.10 to 0.90 cc/g and a pore diameter distribution in which the pore diameters are distributed concentratedly in the ranges of from 0.1 to less than 1.0 μm, from 1.0 to less than 10.0 μm and from 10.0 to 100 μm. The catalyst can be prepared, with good reproducibility, by charging an unfired catalyst material powder composition into a centrifugal flow coating apparatus to form particles having an average diameter of 2 to 10 mm, and then firing the particles.

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This invention relates to a catalyst suitable for the production of acrylic acid from acrolein, which comprises molybdenum and vanadium as essential components, and a process for the preparation thereof. More specifically, this invention relates to a catalyst for the oxidation of acrolein, which has high activity and excellent durability and which is characterized by specific properties, and a process for the preparation of said catalyst with ease and good reproducibility.

There are many literatures proposing various catalysts for producing acrylic acid at high yields by a catalytic gas phase oxidation reaction of acrolein. These proposals are mainly concerned with selection of components for catalysts and proportions thereof. Some of them are also concerned with selection of catalyst properties and production processes with reproducibility. Although there are not a few proposals concerning catalyst properties such as surface area, pore volume, etc., none of these proposed catalysts are found to be on a satisfactory level.

For example, as a disclosure of the surface area, it is described in Japanese Laid-Open Patent Publications Nos. 86812/1973 and 91010/1973 that the catalyst surface areas of 0.1 to 50 m²/g are preferable. However, those catalysts described therein have defects of high reaction temperatures and low level of performance. Japanese Laid-Open Patent Publications Nos. 47276/1974 and 24183/1975 describe that the specific surface areas of 0.1 to 8 m²/g are preferable. However, those catalysts described therein also have a defect of high reaction temperatures as high as about 300° C. With regard to the definition of the pore volume and surface area, it is described in Japanese Laid-Open Patent Publications Nos. 65395/1974 and 62409/1974 that the surface areas of 4 to 8 m²/g and pore volumes of 0.1 to 0.2 ml/g are preferable. However, those catalysts described therein comprise cobalt and molybdenum as active components and they are technically on a low level.

Japanese Laid-Open Patent Publication No. 47590/1976 describes that a catalyst comprising phosphorus, molybdenum and thallium or an element of Group IA or II of the periodic table and formed by rolling particle-forming method so as to have a surface area of 4 to 20 m²/g and a pore volume of 0.08 to 0.5 ml/g has reproduction in performance. However, this catalyst also has defects that the reaction temperature is high and the performance is unsatisfactory. Japanese Laid-Open Patent Publication No. 9737/1982 discloses a catalyst comprising, as essential components, molybdenum, vanadium, copper, iron, manganese, alkali earth metal or zinc, and oxygen and further including phosphorus as an optional component, and a process for the production of acrylic acid by using said catalyst in the oxidation of acrolein. And it discloses an embodiment of the catalyst in which an alundum having a diameter of 3.5 mm is allowed to carry catalyst components by a rotatory sugar coater. In the catalyst therein, the reaction temperature is relatively low, i.e., about 200° C, and said catalyst achieves a high level in the yields. However, the catalyst obtained by the process has a problem in respect of reproducibility of its properties.

The present inventors have had an idea that the catalyst properties are not determined by the mere definition of catalyst surface area and/or pore volume but that industrially excellent catalysts can be obtained only when the catalysts are imparted with properties resulting from the combination of three factors of catalyst surface area, pore volume and pore diameter distribution. Meanwhile, in the case of carrying out the oxidation reaction of acrolein by the use of a reaction apparatus having a fixed bed or moving bed, catalysts are used, in general, in the form of pellets having a suitable size. Such pellets are formed by using a tablet-forming machine, extruder, pill-forming machine, rolling particle-forming machine, etc. However, the physical property of the resultant catalyst is not constant, that is, most cases show poor reproducibility of catalyst performance. Thus, in such forming methods, it is difficult to obtain catalysts without lowering the catalyst performance.

Therefore, the present inventors made assiduous studies to clear up those variations of catalyst performance which are caused at the time of forming catalysts by using various forming machines. As a result, it was found that in the case of a catalyst material containing Mo, V, A, B, C, D, and O (wherein Mo represents molybdenum, V represents vanadium, A represents at least one element selected from the group consisting of tungsten and niobium, B represents at least one element selected from the group consisting of iron, copper, bismuth, chromium, antimony and thallium, C represents at least one element selected from the group consisting of alkali metals and alkali earth metals, D represents at least one element selected from the group consisting of silicon, aluminum and titanium, and O represents oxygen,) as active components, the catalyst performance lowers to a great extent and the performance and physical property vary depending upon forming methods, and it was also found that the main cause of the foregoing is that since the pores of the catalyst are conditioned at the formation time, the catalyst surface area, pore volume and pore diameter are controlled.

Accordingly, further studies were made with regard to the surface area, pore volume and pore distribution in order to obtain a catalyst comprising the above components and having excellent performance. As a result, it was found that such a catalyst has to satisfy three conditions that it has a surface

area of 0.50 to 15.0 m²/g, that it has a pore volume of 0.10 to 0.90 cc/g and that it has a pore diameter distribution in which the pore diameters are distributed concentratedly in the ranges of from 0.1 to less than 1.0 μ m, from 1.0 to less than 10.0 μ m and from 10 to 100 μ m. The pore volume composed of pores having pore diameters in the range of from 0.1 to less than 1.0 μ m is not less than 10 % of the entire pore volume, especially preferably, 15 to 40 %, and the pore volumes composed of pores having pore diameters in the range of from 1.0 to less than 10.0 μ m and pores having pore diameters in the range from 10.0 to 100 μ m are not less than 10 % of the entire pore volume respectively, especially preferably, 15 to 65 % respectively. It was found that when these conditions are satisfied, both of the activity and the selectivity of the above catalyst are enhanced. That is, a pore having a smaller pore diameter, e.g., less than 1.0 μ m, has a larger contribution toward the surface area and pore volume. However, in the pores having a contribution toward the activity and selectivity to the effective reaction product, the mere larger proportion of the smaller pores is not sufficient. And if there is not a distribution in which pores are also distributed in two ranges of from 1.0 to less than 10.0 μ m and from 10.0 to 100 μ m, it is not possible to obtain enhancement of the performance.

On the basis of the above finding, the present inventors diligently continued the studies and consequently found that the use of a centrifugal flow coating apparatus in shaping of an unfired catalyst powder not formed into particles can give catalysts which are excellent in reproducibility and exhibit excellent catalyst performance.

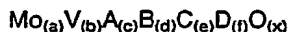
In usual formation methods of catalysts, a rolling particle-forming method, marmerizer-forming method, fluidized bed particle-forming method, etc., are used for the preparation of spherical shapes, and an extrusion method, tablet-forming method, etc., are used for cylindrical shapes. However, in the case of using these formation methods, it is difficult in many cases to form catalysts without degrading the catalyst performance, the performance frequently varies widely and the reproducibility is often poor. In contrast thereto, in the use of a centrifugal flow coating apparatus according to this invention, the apparatus is simply operated and gives good producibility and it is possible to prepare spherical or particulate catalysts. Further, the formation by a centrifugal flow coating apparatus also has advantages that catalysts having a narrow distribution of particle size can be obtained and that, since said catalysts are particulate or spherical, the catalysts have high mechanical strength, little pressure loss and high resistance to friction and are easy to fill in or take out from a reaction apparatus.

Meanwhile, the use of a centrifugal flow coating device is known as one method of forming particles from powder material. For example, Japanese Patent Publication No. 10878/1971 discloses said use with regard to a case where pharmaceutical compositions are sugar-coated. Japanese Patent Publication No. 17292/1977 also discloses it with regard to a case where particulate cores are coated with a catalyst and/or carriers.

In this invention, this method is applied to the preparation of the above-mentioned oxide catalyst. According to the process of this invention, it is possible to easily obtain a spherical or particulate catalyst having the aforespecified surface area, pore volume and pore diameter distribution and having high physical strength by only using water as a binder or by optionally using, in combination therewith, a substance which imparts the catalyst with pores by combustion or volatilization at the time of firing. The catalyst of this invention can be produced, for example, by charging an unfired catalyst material powder composition into a centrifugal flow coating apparatus to form particles with blowing heated air thereinto and spraying a binder such as water, taking out particles grown to the desired size in batch-type operation or in successive operation, then drying the particles as necessary and thereafter firing them at a temperature of 200 to 500 °C, preferably 300 to 450 °C.

The catalyst of this invention can be used directly as such, or by diluting it with an inert carrier or in the state in which the catalyst is held in said carrier. In the formation of the particles, it is preferable to use, as a core, granules obtained by preforming a catalyst per se to a size more than 10 times larger than the particle size of the material powder. Naturally, an inert carrier can be also used as this core. Examples of the inert carrier include silicon carbide, silica, alpha-alumina and others known as a refractory material. With regard to a coating catalyst powder to grow a particle diameter, it is preferable to preadjust the powder to not more than 100 mesh. In order to prepare a catalyst having the surface area, pore volume and pore diameter distribution specified by this invention with good reproducibility, for example, a polyvinyl alcohol, stearic acid, etc., may be added to the catalyst material powder composition at the time of preparing said composition or at the time of shaping. As a binder of the powder, it is also possible to use water, ammonium nitrate, graphite, starch, etc., and organic solvents such as alcohol, acetone, etc., can be used as well.

The chemical composition of the catalyst of this invention is known in itself and is represented by the following general formula



(wherein Mo represents molybdenum, V represents vanadium, A represents at least one element selected from the group consisting of tungsten and niobium, B represents at least one element selected from the group consisting of iron, copper, bismuth, chromium, antimony and thallium, C represents at least one element selected from the group consisting of alkali metals and alkali earth metals, D represents at least one element selected from the group consisting of silicon, aluminum and titanium, and O represents oxygen; and further, a, b, c, d, e, f and x represent atomic ratios of Mo, V, A, B, C, D, and O respectively, and when a = 12, then b = 2 to 14, c = 0 to 12, d = 0 to 6, e = 0 to 6 and f = 0 to 30 and x is a numerical value determined depending upon the oxidation states of the other elements).

A catalytic gas phase oxidation reaction of this invention is carried out by introducing a material gas composed of 1 to 10 % by volume of acrolein, 1 to 15 % by volume of molecular oxygen, 5 to 60 % by volume of water vapor and 20 to 80 % by volume of an inert gas (e.g., a mixed gas consisting of nitrogen, carbonic acid gas, saturated hydrocarbon gas, etc.) onto the catalyst at a temperature in the range of from 150 to 400 °C at a pressure of atmospheric pressure to 10 atm and at a space velocity of 500 to 20,000 hr⁻¹ (STP). In addition, as a material gas, an acrolein-containing gas obtained by catalytic reaction of propylene may be also used directly.

The following Examples and Comparative Examples illustrate this invention more in detail. However, this invention shall not be limited to these Examples. In this invention, the conversion ratio and the yield in a single flow are respectively defined as follows.

Conversion ratio (%) =

$$\frac{\text{Number of moles of reacted acrolein}}{\text{Number of moles of charged acrolein}} \times 100$$

Yield in a single flow (%) =

$$\frac{\text{Number of moles of produced acrylic acid}}{\text{Number of moles of charged acrolein}} \times 100$$

Example I (Preparation of suspension of catalyst material)

While 50 liters of water was stirred under heat, dissolved therein were 1,560 g of ammonium paratungstate, 1,290 g of ammonium metavanadate, 5,070 g of ammonium molybdate and 180 g of ammonium dichromate to prepare an aqueous solution. Separately, 1,290 g of copper nitrate was dissolved in 3.0 liters of water to prepare another aqueous solution. These two solutions were mixed, and the mixture solution was heated and stirred to give a suspension. (The suspension is referred to as a suspension-A.)

Example I-1-1

(Preparation of a catalyst by a centrifugal flow coating method)

A part of the suspension A was evaporated to dry solidness with stirring under heat. Then the resultant solid in the block state was dried in a drier at 120 °C for 5 hours, and milled to about 100 mesh to give a powder. Alpha-alumina particles having an average diameter of 1 mm was first charged to a centrifugal flow coating apparatus. Then the above powder was charged thereto together with distilled water as a binder with blowing heated air at 90 °C, and spherical particles having an average diameter of 5 mm were formed. The spherical particles obtained as above were fired at a temperature of 400 °C for 5 hours. The compositional ratio of the elements except oxygen in the resultant catalyst oxide was Mo₍₁₂₎V_(4.6)Cu_(2.2)Cr_(0.6)W_(2.4). This catalyst is referred to as a catalyst (I-1-1).

Example I-1-2

5 (Preparation of a catalyst by a centrifugal flow coating method)

Example I-1-1 was repeated except that 40 wt.% ammonium nitrate aqueous solution was used as a binder in place of water, and a catalyst (I-1-2) was obtained.

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Examples I-2-1 and I-2-2

15 (Preparation of catalysts by tablet-forming method)

A part of the suspension-A was evaporated to dry solidness with stirring under heat. Then the resultant solid in the block state was dried in a drier under air current at 120° C for 5 hours, and the dried block was milled to not more than 100 mesh to give a powder. 2 % by weight of a carbon powder was added to the
20 powder, and the resultant mixture was formed into tablets having a diameter of 5 mm and height of 5 mm. The tablets were fired at 400° C for 5 hours to prepare a catalyst (I-2-1). The same procedure was repeated to prepare another catalyst (I-2-2).

25 Examples I-3-1 and I-3-2

(Preparation of a catalyst by extrusion method)

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A part of the suspension-A was concentrated by evaporation until it could be extruded, and extruded so as to form extrudates having a diameter of 5 mm and length of 5 mm. The extrudates were fired at 400° C for 5 hours to prepare a catalyst (I-3-1). The same procedure was repeated to prepare another catalyst (I-3-2).

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Example I-4

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(Preparation of a catalyst by marmerizerforming method)

A part of the suspension-A was subjected to concentrating heat treatment by external heat to concentrate it until it could be extruded. The concentrate was extrusion-molded to form extrudates having a
45 diameter of 6 mm and length of 4 to 7 mm. Then the extrudates were subjected to a marmerizer to form 3 mm x 5 mm spheroids. The spheroids were fired at 400° C for 5 hours to prepare a catalyst (I-4).

Example I-5

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(Preparation of a catalyst by rolling particle-forming method)

A part of the suspension-A was evaporated to dry solidness with stirring under heat. Then the resultant solid in the block state was dried in a drier at 120 °C for 5 hours, and the dried block was milled to about 100 mesh to obtain a powder. Alpha-alumina particles having an average diameter of 1 mm were charged first into a rolling particle-forming machine. And then the above powder was charged therein, and heated air at 80 °C and distilled water as a binder were used to form spheres having an average diameter of 5 mm. The spheres were fired at 400 °C for 5 hours to prepare a catalyst (I-5).

Example I-6

(Preparation of a catalyst by pill-forming method)

A part of the suspension-A was subjected to concentrating heat treatment by externally heating to obtain a soil-like substance, 50 % by weight of which was dissipated when it was fired at 400 °C. The soil-like substance was formed by a pill-forming machine into spheres having an average diameter of 5 mm. The spheres were fired at 400 °C for 5 hours to prepare a catalyst (I-6).

[Reaction Test]

The activity test on each of the above catalysts I-1 to I-6 was carried out in the following procedure.

1,000 ml of the catalyst was charged to a steel reaction tube having an internal diameter of 25.4 mm, and a mixture gas obtained by catalytic gas phase oxidation of industrial-use propylene (having a purity of not less than 95 %) in the presence of a catalyst of a molybdenum/ cobalt/tungsten oxide type was introduced therein to carry out the reaction at a reaction temperature of 200 to 250 °C and at a space velocity of 3,000hr⁻¹. The average composition of the mixture gas for the reaction was as follows.

Acrolein	5.64 % by volume
Propylene + propane	0.65 % by volume
Acrylic acid + acetic acid	0.74 % by volume
Nitrogen	70.03 % by volume
Water vapor	17.22 % by volume
Oxygen	4.75 % by volume
Others	0.97 % by volume

Example I-1-3

An 8,000 hour-successive reaction test was carried out by the use of the catalyst of Example I-1-1. The procedure for the reaction test was the same as in Example I. The temperature in the beginning of the reaction was 200 °C, however, it was sufficient to elevate the temperature by 5 °C during the period of time of 8,000 hours. The reaction results at the reaction temperature of 205 °C were that the acrolein conversion ratio was 99.6 % and the yield of acrylic acid in a single flow was 97.0 %.

Example I-7

(Preparation of a catalyst on a carrier)

A part of the suspension-A was charged into an evaporator on a hot water bath, and added thereto was a particulate alpha-alumina carrier having a specific surface area of $1 \text{ m}^2/\text{g}$, a porosity of 42 %, a pore distribution, 92% of which was made by pores having diameters of 75 to 250 microns, and diameters of 3. to 5 mm. The mixture was evaporated to dry solidness with stirring, and then fired at 400°C for 5 hours to prepare a catalyst (I-7). The reaction test was carried out in the same way as in Examples I-1 to I-6.

Table 1 shows physical properties and activities measured with regard to the catalysts I-1 to I-7.

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Table - 1

Ex- ample	Forming method	Surface area m^2/g	Pore volume cc/g	Pore distribution			Reaction temperature (°C)	Acrolein conversion ratio	Yield of acrylic acid in a single flow
				*1 A	*2 B	*3 C			
I-1-1	Centrifugal flow coating method	4.7	0.250	22	21	55	210	99.8	97.1
I-1-2	"	4.8	0.247	23	22	54	200	99.6	97.5
I-2-1	Tablet-forming method	2.7	0.150	-	25	70	210	90.6	75.2
I-2-2	"	2.0	0.110	-	21	74	210	85.3	72.5
I-3-1	Extrusion method	3.5	0.170	-	30	68	210	92.4	84.1
I-3-2	"	3.2	0.163	-	35	60	210	89.8	82.6
I-4	Marmerizer-forming method	3.7	0.160	-	31	65	210	90.1	83.3
I-5	Rolling particle forming method	4.1	0.210	6	30	60	210	94.8	90.1
I-6	Pill-forming method	4.7	0.220	8	28	62	210	93.2	88.5
I-7	Carrier added-forming method	1.50	0.180	-	40	55	210	87.4	87.0

*1 Ratio (%) of pore volume consisting of pores having diameters in the range of from 10 to 100 μm to the entire pore volume.

(The asterisk in the other Tables means the same.)

*2 Ratio (%) of pore volume consisting of pores having diameters in the range of from 1 to less than 10 μm to the entire pore volume.

(The asterisk in the other Tables means the same.)

*3 Ratio (%) of pore volume consisting of pores having diameters in the range of from 0.1 to less than 1 μm to the entire pore volume.

(The asterisk in the other Tables means the same.)

Example II

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(Preparation of a catalyst and test on reproducibility thereof)

10 A suspension was prepared in the same way as in Example 1 and divided into four equal portions for four batches. From these four batches, powders or clay-like substances were prepared as materials suitable for various forming methods. The materials were formed into catalysts in the same way as in Examples I-1 to I-7 series, and the reproducibility in the same forming method was examined by comparing the performances. In the same forming method, catalysts of the four batches were prepared independently of one
15 another in the same procedure and under the same conditions. The performance tests were carried out according to the procedure of Examples I-1 to I-7 series except that the test in Example II-1 was carried out according to Example I-1-1.

The results are shown in Table 2.

20 As is clear in Table 2, catalysts resulting from formation by centrifugal coating method have a smaller variation in values of physical property and high activity in catalyst performance, and it is seen on the basis of the smaller variation that the catalysts were prepared with good reproducibility. On the other hand, it is further seen that the other formation methods in some batches give catalysts which do not have the surface area, pore volume and pore distribution specified by this invention, although the catalysts were prepared under the same conditions, and that, as method for obtaining catalysts having good performance with good
25 reproducibility, these other forming methods are inferior to the centrifugal flow coating method.

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Table - 2

Ex- ample	Forming method	Batch No.	Surface area m ² /g	Pore volume cc/g	Pore distribution			Reaction tempera- ture (°C)	Acrolein conver- sion ratio	Yield of acrylic acid in a single flow
					*1 A	*2 B	*3 C			
II-1	Centrifugal flow coating method	1	4.7	0.246	23	23	52	210	99.6	97.4
	"	2	4.8	0.252	23	20	54	210	99.7	97.3
	"	3	4.9	0.251	21	21	56	210	99.6	97.5
	"	4	4.6	0.251	24	22	52	210	99.5	97.4
II-2	Tablet-forming method	1	2.5	0.170	-	20	77	210	89.8	76.7
	"	2	2.0	0.160	-	23	76	210	87.1	74.9
	"	3	2.9	0.200	-	29	68	210	92.0	77.4
	"	4	2.3	0.171	-	27	72	210	90.3	75.5
II-3	Extrusion method	1	3.0	0.185	-	31	66	210	90.7	83.4
	"	2	3.2	0.190	-	30	65	210	89.8	84.4
	"	3	2.7	0.153	-	25	74	210	86.1	80.9
	"	4	3.4	0.216	-	42	56	210	95.2	87.1
II-4	Marmerizer-forming method	1	3.3	0.186	-	35	61	210	91.3	85.8
	"	2	3.5	0.211	-	32	67	210	89.1	84.6
	"	3	2.6	0.200	-	23	73	210	85.7	79.7
	"	4	2.9	0.217	-	25	74	210	87.3	81.7

- to be continued -

Table - 2 (continued)

Ex-ample	Forming method	Batch No.	Surface area m ² /g	Pore volume cc/g	Pore distribution			Reaction temperature (°C)	Acrolein conversion ratio	Yield of acrylic acid in a single flow
					#1 A	#2 B	#3 C			
II-5	Rolling particle forming method	1	4.8	0.230	6	31	60	210	95.2	90.7
	"	2	3.9	0.210	4	32	62	210	96.0	91.5
	"	3	4.3	0.189	3	25	71	210	97.3	92.0
	"	4	4.4	0.214	7	42	47	210	94.7	90.8
II-6	Pill-forming method	1	4.8	0.220	3	25	71	210	92.6	88.9
	"	2	5.1	0.217	4	27	65	210	94.7	90.9
	"	3	4.0	0.169	2	23	74	210	90.5	87.8
	"	4	4.6	0.182	7	31	61	210	91.7	85.3
II-7	Carrier added-forming method	1	1.7	0.153	-	41	58	210	86.2	84.5
	"	2	1.9	0.193	-	57	40	210	93.1	89.4
	"	3	1.2	0.167	-	40	59	210	87.3	85.9
	"	4	1.6	0.148	-	51	47	210	85.1	82.8

Example III

(Preparation of material suspension for catalyst)

While 6.0 liters of water was heated with stirring, 234.0 g of ammonium metavanadate and 1,059.4 g of ammonium molybdate were dissolved in the water to prepare an aqueous solution. Separately, 241.6 g of copper nitrate and 40.4 g of ferric nitrate were dissolved in water to prepare another aqueous solution. These two aqueous solution were mixed. And further, added to the resulting solution was 134 ml of 20 % by weight of SiO₂-containing silica sol as a carrier to form a suspension. (The suspension is referred to as suspension-B.)

Example III-1

(Preparation of a catalyst by centrifugal flow coating method)

A part of the suspension-B was treated in the same way as in Example I-1-1 to prepare a catalyst. However, the firing was carried out at 400 °C for 6 hours. The compositional ratio of the elements except oxygen in the resultant catalyst oxide was Mo_(1.2)V₍₄₎Cu₍₂₎Fe_(0.2)Si_(1.0).

Examples III-2-1 and III-2-2

(Preparation of catalysts by tablet-forming method)

A part of the suspension-B was treated in the same way as in Example I-2 to prepare catalysts. However, the firing was carried out at 400 °C for 6 hours.

[Reaction test]

By the use of the catalysts of Examples III-1 to III-2, the reactions were carried out in the same way as in Example I, except that the reaction temperature was set at 230 °C.

Example IV

(Preparation of material suspension for catalyst)

Ammonium molybdate (1,596 g) was dissolved in 12 liters of water under heat. 220.8 g of ammonium metavanadate, 1,126.5 g of niobium hydroxide, 162 g of ferrous oxalate, 88.5 g of cuprous chloride and 45 g of potassium nitrate were consecutively added to the above solution with fully stirring. After the mixture was heated with stirring, 678 g of an SiO₂ powder was added to prepare a suspension. (This suspension is referred to as a suspension-C.)

Example IV-1

(Preparation of a catalyst by centrifugal flow coating method)

A part of the suspension-C was treated in the same way as in Example I-1-1 to prepare a catalyst except that the firing was carried out at 420 °C for 5 hours. The compositional ratio of the elements except oxygen in the resultant catalyst oxide was



Examples IV-2-1 and IV-2-2

(Preparation of catalysts by extrusion method)

A part of the suspension-C was treated in the same way as in Example I-3 to prepare catalysts. However, the firing was carried out at 420 °C for 5 hours.

[Reaction test]

By the use of the catalysts of Examples IV-1 to IV-2, the reactions were carried out in the same way as in Example I, except that the reaction temperature was set at 240 °C.

Example V

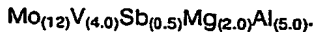
(Preparation of material suspension for catalyst)

A suspension was obtained in the same way as in Example I. There were used antimony pentoxide as an antimony source, a nitrate as a magnesium source and an oxide as an aluminum source. (This suspension is referred to as a suspension-D.)

Example V-1

(Preparation of a catalyst by centrifugal flow coating method)

A part of the suspension-D was treated in the same way as in Example I-1-1 to prepare a catalyst. The compositional ratio of the elements except oxygen in the resultant catalyst oxide was



Examples V-2-1 and V-2-2

(Preparation of catalysts by marmerizer-forming method)

A part of the suspension-D was treated in the same way as in Example I-4 to prepare catalysts.

[Reaction test]

By the use of the catalysts of Examples V-1 to V-2, the reactions were carried out in the same way as in Example I, except that the reaction temperature was set at 240 ° C.

Example VI

(Preparation of material suspension for catalyst)

A suspension was obtained in the same way as in Example I. As a cesium source and strontium source, nitrates were used, and as a titanium source, an oxide was used. (This suspension is referred to as a suspension-E.)

Example VI-1

(Preparation of a catalyst by centrifugal flow coating method)

A part of the suspension-E was treated in the same way as in Example I-1-1 to prepare a catalyst. The compositional ratio of the elements except oxygen in the resultant catalyst oxide was $\text{Mo}_{(12)}\text{V}_{(4)}\text{W}_{(2.0)}\text{Sr}_{(2.0)}\text{Ti}_{(10)}$.

Examples VI-2-1 and VI-2-2

(Preparation of a catalyst by rolling particle-forming method)

A part of the suspension-E was formed into catalysts according to Example I-5.

[Reaction test]

By the use of the catalysts of Examples VI-1 to VI-2, the reactions were carried out in the same way as in Example I, except that the reaction temperature was set at 220 ° C.

Example VII

(Preparation of material suspension for catalyst)

A suspension was obtained in the same way as in Example I. Additionally used were ferric nitrate as an iron source, sodium nitrate as a sodium source and an oxide as an aluminum source. (This suspension is referred to as a suspension-F.)

Example VII-1

(Preparation of a catalyst by centrifugal flow coating method)

A part of the suspension-F was treated in the same way as in Example I-1-1 to prepare a catalyst. The compositional ratio of the elements except oxygen in the resultant catalyst oxide was

5 $\text{Mo}_{(1.2)}\text{V}_{(8.0)}\text{W}_{(4.0)}\text{Cu}_{(1.0)}\text{Fe}_{(1.0)}\text{Na}_{(0.5)}\text{Al}_{(5.0)}$.

Examples VII-2-1 and VII-2-2

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(Preparation of a catalyst by pill-forming method)

A part of the suspension-F was formed into catalysts according to Example I-6.

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[Reaction test]

20 By the use of the catalysts of Examples VII-1 to VII-2, the reactions were carried out in the same way as in Example I, except that the reaction temperature was set at 210° C.

Example VIII

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(Preparation of material suspension for catalyst)

30 A suspension was obtained in the same way as in Example I. In addition, there were used nitrates as bismuth and rubidium sources and silica gel as a silicon source. (This suspension is referred to as a suspension-G).

Example VIII-1

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(Preparation of a catalyst by centrifugal flow coating method)

40 A part of the suspension-G was treated in the same way as in Example I-1-1 to prepare a catalyst. The compositional ratio of the elements except oxygen in the resultant catalyst oxide was

$\text{Mo}_{(1.2)}\text{V}_{(8.0)}\text{W}_{(4.0)}\text{Cu}_{(1.0)}\text{Bi}_{(1.0)}\text{Rb}_{(0.05)}\text{Si}_{(5.0)}$.

Examples VIII-2-1 and VIII-2-2

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(Preparation of a catalyst by carrier-added forming method)

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A part of the suspension-G was formed into catalysts according to Example I-7.

[Reaction test]

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By the use of the catalysts of Examples VIII-1 to VIII-2, the reactions were carried out in the same way as in Example I.

Example IX

5 (Preparation of material suspension for catalyst)

A suspension was obtained in the same way as in Example I. In addition, there were used nitrates as bismuth and cesium sources and silica gel as a silicon source. (This suspension is referred to as a suspension-H.)

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Example IX-1

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(Preparation of a catalyst by centrifugal flow coating method)

A part of the suspension-H was treated in the same way as in Example I-1-1 to prepare a catalyst. The compositional ratio of the elements except oxygen in the resultant catalyst oxide was

20 $\text{Mo}_{(1.2)}\text{V}_{(8.0)}\text{W}_{(1.0)}\text{Bi}_{(1.0)}\text{X}_{(0.05)}\text{Si}_{(5.0)}$.

Examples IX-2-1 and IX-2-2

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(Preparation of a catalyst by tablet-forming method)

A part of the suspension-H was formed into catalysts according to Example I-2.

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[Reaction test]

35 By the use of the catalysts of Examples IX-1 to IX-2, the reactions were carried out in the same way as in Example I.

The results of the above Examples III to IX are summarized in Table 3.

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Table - 3

Ex- ample	Forming method	Surface area m ² /g	Pore volume cc/g	Pore distribution			Reaction temperature (°C)	Acrolein conversion ratio	Yield of acrylic acid in a single flow
				*1 A	*2 B	*3 C			
III-1	Centrifugal flow coating method	5.0	0.283	21	30	48	230	96.8	92.9
III-2-1	Tablet-forming method	3.1	0.216	-	25	70	230	92.0	84.6
III-2-2	"	2.2	0.179	-	17	82	230	88.5	82.3
IV-1	Centrifugal flow coating method	6.3	0.324	18	33	48	240	94.3	90.5
IV-2-1	Extrusion method	4.1	0.261	-	42	57	240	91.7	85.5
IV-2-2	"	2.9	0.215	-	30	69	240	88.4	80.6
V-1	Centrifugal flow coating method	4.1	0.305	16	32	49	240	98.7	89.8
V-2-1	Marmerizer-forming method	3.9	0.213	-	31	66	240	92.5	81.4
V-2-2	"	2.6	0.192	-	46	53	240	89.8	82.6
VI-1	Centrifugal flow coating method	4.2	0.295	19	27	50	220	99.6	95.6
VI-2-1	Rolling particle forming method	4.7	0.281	7	40	50	220	95.1	91.3
VI-2-2	"	3.6	0.325	3	23	71	220	92.6	89.8

-- to be continued --

Table - 3 (continued)

Ex- ample	Forming method	Surface area m^2/g	Pore volume cc/g	Pore distribution			Reaction temperature (°C)	Acrolein conversion ratio	Yield of acrylic acid in a single flow
				*1 A	*2 B	*3 C			
VII-1	Centrifugal flow coating method	5.6	0.371	23	34	40	220	99.1	95.5
VII-2-1	Pill-forming method	4.1	0.257	3	21	71	220	93.4	89.7
VII-2-2	"	4.9	0.326	9	18	69	220	96.7	90.9
VIII-1	Centrifugal flow coating method	4.3	0.310	35	20	41	210	97.8	94.9
VIII-2-1	Carrier added-forming method	1.2	0.126	-	44	51	210	86.9	82.6
VIII-2-2	"	1.8	0.192	-	50	48	210	89.3	83.9
IX-1	Centrifugal flow coating method	4.3	0.256	21	29	49	210	97.9	94.0
IX-2-1	Tablet-forming method	2.1	0.169	-	21	76	210	91.6	87.9
IX-2-2	"	3.3	0.217	-	30	68	210	94.3	88.9

Example X-1

(Preparation of catalyst by a centrifugal flow coating method)

Example I-1-1 was repeated except that alpha-alumina particle having an average diameter of 3 mm was first charged to a centrifugal flow coating apparatus as a core in place of alpha-alumina particle having an average diameter of 1 mm.

Example X-2

Example X-1 was repeated except that alpha-alumina particle having an average diameter of 5 mm was first charged as a core.

[Reaction test]

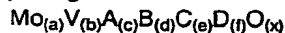
By the use of the catalysts of Examples X-1 to X-2, the reaction was carried out in the same way as in Example I. The reaction results at the reaction temperature of 210°C were that the acrolein conversion ratio was 99.6% and the yield of acrylic acid in a single flow was 97.2% for Example X-1 and the acrolein conversion ratio was 99.4% and the yield of acrylic acid in a single flow was 97.3% for Example X-2.

As for Example X-1, surface area was 4.0 m²/g, and pore volume was 0.237 cc/g, and the ratio of pore volume consisting of pores having diameters in the range of from 10 to 100 μm, from 1 to less than 10 μm, from 0.1 to less than 1 μm to the entire pore volume were 22%, 20% and 48% respectively.

As for Example X-2, surface area was 2.5 m²/g, and pore volume was 0.185 cc/g, and the ratio of pore volume consisting of pores having diameters in the range of from 10 to 100 μm, from 1 to less than 10 μm, from 0.1 to less than 1 μm to the entire pore volume were 22%, 21% and 55% respectively.

Claims

1. A catalyst for use in the production of acrylic acid by catalytic gas phase oxidation of acrolein, comprising active substances represented by general formula

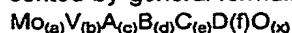


wherein Mo represents molybdenum, V represents vanadium, A represents at least one element selected from the group consisting of tungsten and niobium, B represents at least one element selected from the group consisting of iron, copper, bismuth, chromium, antimony and thallium, C represents at least one element selected from the group consisting of alkali metals and alkali earth metals, D represents at least one element selected from the group consisting of silicon, aluminum and titanium, and O represents oxygen; and further, a, b, c, d, e, f and x represent atomic ratios of Mo, V, A, B, C, D, and O respectively, and when a=12, then b=2 to 14, c=0 to 12, d=0 to 6, e=0 to 6 and f=0 to 30 and x is a numerical value determined depending upon the oxidation states of the other elements, and characterized by having a specific surface area of 0.50 to 15.0 m²/g, a pore volume of 0.10 to 0.90 cc/g and a pore diameter distribution in which the pore diameters are distributed concentratedly in the ranges of from 0.1 to less than 1.0 μm, from 1.0 to less than 10.0 μm and from 10.0 to 100 μm.

2. A catalyst according to claim 1 wherein the pore volume composed of pores having pore diameters in the range of from 0.1 to less than 1.0 μm, the pore volume composed of pores having pore diameters in the range of from 1.0 to less than 10.0 μm and the pore volume composed of pores having pore diameters in the range of from 10 to 100 μm are respectively at least 10 % based on the entire pore volume.

3. A catalyst according to claim 1 wherein the pore volume composed of pores having pore diameters in the range of from 0.1 to less than 1.0 μm , the pore volume composed of pores having pore diameters in the range of from 1.0 to less than 10.0 μm and the pore volume composed of pores having pore diameters in the range of from 10 to 100 μm are respectively 15 to 40 %, 15 to 65 % and 15 to 65 % based on the entire pore volume.

4. In a process for preparation, with good reproducibility, of a catalyst which is used in the production of acrylic acid by catalytic gas phase oxidation of acrolein and which comprises active substances represented by general formula



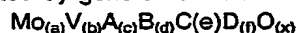
wherein Mo represents molybdenum, V represents vanadium, A represents at least one element selected from the group consisting of tungsten and niobium, B represents at least one element selected from the group consisting of iron, copper, bismuth, chromium, antimony and thallium, C represents at least one element selected from the group consisting of alkali metals and alkali earth metals, D represents at least one element selected from the group consisting of silicon, aluminum and titanium, and O represents oxygen; and further, a, b, c, d, e, f and x represent atomic ratios of Mo, V, A, B, C, D, and O respectively, and when $a=12$, then $b=2$ to 14, $c=0$ to 12, $d=0$ to 6, $e=0$ to 6 and $f=0$ to 30 and x is a numerical value determined depending upon the oxidation states of the other elements; the process characterized by charging an unfired catalyst material powder composition into a centrifugal flow coating apparatus to form particles having an average diameter of 2 to 10 μm , and then firing the particles thereby to obtain the catalyst having a specific surface area of 0.50 to 15.0 m^2/g , a pore volume of 0.10 to 0.90 cc/g and a pore diameter distribution in which the pore diameters are distributed concentratedly in the ranges of from 0.1 to less than 1.0 μm , from 1.0 to less than 10.0 μm and from 10.0 to 100 μm .

5. A process according to claim 4 for the preparation of a catalyst in which the pore volume composed of pores having pore diameters in the range of from 0.1 to less than 1.0 μm , the pore volume composed of pores having pore diameters in the range of from 1.0 to less than 10.0 μm and the pore volume composed of pores having pore diameters in the range of from 10 to 100 μm are respectively at least 10 % based on the entire pore volume.

6. A process according to claim 4 for the preparation of a catalyst in which the pore volume composed of pores having pore diameters in the range of from 0.1 to less than 1.0 μm , the pore volume composed of pores having pore diameters in the range of from 1.0 to less than 10.0 μm and the pore volume composed of pores having pore diameters in the range of from 10 to 100 μm are respectively 15 to 40 %, 15 to 65 % and 15 to 65 % based on the entire pore volume.

Claims for the following Contracting State: ES

1. In a process for preparation, with good reproducibility, of a catalyst which is used in the production of acrylic acid by catalytic gas phase oxidation of acrolein and which comprises active substances represented by general formula



wherein Mo represents molybdenum, V represents vanadium, A represents at least one element selected from the group consisting of tungsten and niobium, B represents at least one element selected from the group consisting of iron, copper, bismuth, chromium, antimony and thallium, C represents at least one element selected from the group consisting of alkali metals and alkali earth metals, D represents at least one element selected from the group consisting of silicon, aluminum and titanium, and O represents oxygen; and further, a, b, c, d, e, f and x represent atomic ratios of Mo, V, A, B, C, D, and O respectively, and when $a=12$, then $b=2$ to 14, $c=0$ to 12, $d=0$ to 6, $e=0$ to 6 and $f=0$ to 30 and x is a numerical value determined depending upon the oxidation states of the other elements; the process characterized by charging an unfired catalyst material powder composition into a centrifugal flow coating apparatus to form particles having an average diameter of 2 to 10 μm , and then firing the particles thereby to obtain the catalyst having a specific surface area of 0.50 to 15.0 m^2/g , a pore volume of 0.10 to 0.90 cc/g and a pore diameter distribution in which the pore diameters are distributed concentratedly in the ranges of from 0.1 to less than 1.0 μm , from 1.0 to less than 10.0 μm and from 10.0 to 100 μm .

2. A process according to claim 1 for the preparation of a catalyst in which the pore volume composed of pores having pore diameters in the range of from 0.1 to less than 1.0 μm , the pore volume composed of pores having pore diameters in the range of from 1.0 to less than 10.0 μm and the pore volume composed of pores having pore diameters in the range of from 10 to 100 μm are respectively at least 10 % based on the entire pore volume.

3. A process according to claim 4 for the preparation of a catalyst in which the pore volume composed of pores having pore diameters in the range of from 0.1 to less than 1.0 μm , the pore volume composed of pores having pore diameters in the range of from 1.0 to less than 10.0 μm and the pore volume composed of pores having pore diameters in the range of from 10 to 100 μm are respectively 15 to 40 %, 15 to 65 % and 15 to 65 % based on the entire pore volume.

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European Patent
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EUROPEAN SEARCH REPORT

Application Number

EP 88 10 8780

DOCUMENTS CONSIDERED TO BE RELEVANT			
Category	Citation of document with indication, where appropriate, of relevant passages	Relevant to claim	CLASSIFICATION OF THE APPLICATION (Int. Cl. 4)
A	US-A-4 289 654 (BERTOLINI et al.) ----	1-6	B 01 J 23/28
A	FR-A-2 198 920 (MITSUBISHI PETROCHEMICAL CO., LTD) ----		B 01 J 23/88
A	US-A-4 278 566 (HENSLEY et al.) ----		C 07 C 51/25
A	EP-A-0 067 708 (STANSARD OIL CO.) -----		C 07 C 57/04
			B 01 J 35/10
			TECHNICAL FIELDS SEARCHED (Int. Cl. 4)
			B 01 J
			C 07 C
The present search report has been drawn up for all claims			
Place of search THE HAGUE		Date of completion of the search 19-08-1988	Examiner LO CONTE C.
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